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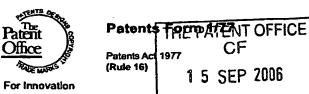
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# An Improved Mist Generating Apparatus and Method

The present invention relates to the field of mist 1 2 generating apparatus. More specifically, the invention is directed to an improved apparatus and 3 method for generating liquid droplet mists. 4 5 6 Mist generating apparatus are known and are used in 7 a number of fields. For example, such apparatus are 8 used in both fire suppression and cooling 9 applications, where the liquid droplet mists generated are more effective than a conventional 10 fluid stream. Examples of such mist generating 11 apparatus can be found in WO2005/082545 and 12 WO2005/082546 to the same applicant. 13 14 A problem with conventional mist generating 15 apparatus is that not all of the working fluid being 16 17 used is atomised as it passes through the apparatus. Although the majority of the working fluid is 18 atomised upon entry into the mixing chamber of the 19 20 apparatus, some fluid is pulled into the chamber but

The non-atomised fluid can stick 1 is not atomised. 2 to the wall of the mixing chamber and flow downstream along the wall to the outlet nozzle, 3 where it can fall into the atomised fluid stream. 4 5 This can cause the creation of droplets which are of 6 non-uniform size. These droplets can then coalesce 7 with other droplets to create still larger droplets, thus increasing the problem and creating a mist of 8 9 non-uniform droplets. 10 11 In cooling applications in particular, the uniformity of the size of the droplets in the mist 12 13 is important. In turbine cooling applications, for example, droplets which are over 10 µm in diameter 14 can cause significant damage to the turbine blades. 15 16 It is therefore important to ensure control and 17 uniformity of droplet size. Optimally sized 18 droplets will evaporate, thus absorbing heat energy 19 and increasing the air density in the turbine. 20 ensures that the efficiency of the turbine is 21 improved. Existing turbine cooling systems employ 22 large droplet eliminators to remove large droplets 23 and thus prevent damage to the turbine. However, 24 such eliminators add to the complexity and 25 manufacturing cost of the apparatus. 26 27 It is an aim of the present invention to obviate or 28 mitigate one or more of the aforementioned 29 disadvantages.

1 According to a first aspect of the present invention there is provided an apparatus for generating a 2 3 mist, comprising: a generally cylindrical body; and an elongate member co-axially located within 5 6 the body such that a first transport fluid passage and a nozzle are defined between the body and the 7 8 elongate member, the first transport fluid passage having a convergent-divergent internal geometry and 9 being in fluid communication with the nozzle; 10 wherein the elongate member includes a working 11 fluid passage and one or more communicating bores 12 13 extending radially outwardly from the working fluid 14 passage, the bores allowing fluid communication between the working fluid passage and the first 15 16 transport fluid passage; and wherein the one or more communicating bores are 17 18 substantially perpendicular to the first transport fluid passage. 19 20 21 Preferably, the communicating bore has an inlet connected to the working fluid passage and an outlet 22 23 connected to the working fluid passage, the outlet having a greater cross-sectional area than the 24 25 inlet. 26 27 The body has an internal wall having an upstream convergent portion and a downstream divergent 28 29 portion, the convergent and divergent portions at least in part forming the convergent-divergent 30 31 internal geometry of the first working fluid passage. A first end of the elongate member has a 32

4

cone-shaped projection, wherein the nozzle is

2 defined between the divergent portion of the 3 internal wall and the cone-shaped projection. 4 one or more communicating bores are adjacent the first end of the elongate member. 5 6 7 Preferably, the cone-shaped projection has a ramped 8 portion extending upwardly from the surface thereof. 9 In a first preferred embodiment, the elongate member 10 11 further includes a second transport fluid passage having an outlet adjacent the end of the cone-shaped 12 projection. Preferably, the first and second 13 transport fluid passages are substantially parallel. 14 15 The second transport fluid passage preferably includes an expansion chamber adjacent its outlet. 16 17 18 In a second preferred embodiment, the bores allowing 19 communication between the working fluid passage and 20 the first transport fluid passage are first bores, 21 and the body further includes a second working fluid 22 passage and one or more second communicating bores allowing fluid communication between the second 23 working fluid passage and the first transport fluid 24 passage. Preferably, the second working fluid 25 26 passage circumscribes the first working fluid 27 passage and the first transport fluid passage. 28 Preferably, the second bores are substantially 29 perpendicular to the first transport fluid passage. 30 Most preferably, the first and second bores are coaxial. 31 32

1 In a third preferred embodiment, the elongate member 2 further includes: 3 a second transport fluid passage circumscribing 4 the working fluid passage; 5 one or more first communicating bores extending 6 radially outwardly from the working fluid passage, 7 the first bores allowing fluid communication between 8 the working fluid passage and the second transport fluid passage; and 9 10 one or more second communicating bores extending radially outwardly from the second 11 12 transport fluid passage, the second bores allowing 13 fluid communication between the second transport 14 fluid passage and the first transport fluid passage; 15 wherein the first and second communicating 16 bores are substantially perpendicular to the second and first transport fluid passages, respectively. 17 18 19 Preferably, the elongate member further includes a 20 third transport fluid passage adapted to supply 21 transport fluid into the second transport fluid 22 passage adjacent the first and second communicating 23 bores. 24 25 Alternatively, the first transport fluid passage 26 communicates with the nozzle via an outlet and a 27 second transport fluid passage in fluid 28 communication with the outlet, wherein the second 29 transport fluid passage has a convergent-divergent. 30 internal geometry and is substantially perpendicular to the first transport fluid passage. 31 32

	the transfer of the transfer o
2	comprises a mixing chamber located between the first
3	transport fluid passage and the nozzle, and a second
4	transport fluid passage in communication with the
5	mixing chamber and the first transport fluid
6	passage, wherein the second transport fluid passage
7	is adapted to supply transport fluid to the mixing
8	chamber in a direction of flow substantially opposed
9	to a direction of flow of transport fluid from the
10	first transport fluid passage.
11	
12	According to a second aspect of the invention, there
13	is provided a method of generating a mist, the
14	method comprising the steps of:
15	supplying a working fluid through a working
16	fluid passage;
17	supplying a first transport fluid through a
18	first transport fluid passage;
19	forcing the working fluid from the working
20	fluid passage into the first transport fluid passage
21	via one or more communicating bores extending
22	radially outwardly from the working fluid passage;
23	accelerating the first transport fluid upstream
24	of the communicating bores so as to provide a high
25	velocity transport fluid flow; and
26	applying the high velocity transport fluid flow
27	to the working fluid exiting the communicating
28	bores, thereby imparting a shear force on the
29	working fluid and atomising the working fluid to
30	produce a dispersed droplet flow regime;

1	wherein the high velocity transport fluid flow
2	is applied substantially perpendicular to the
3	working fluid flow exiting the bores.
4	
-5	Preferably, the method further includes the steps
6	of:
7	forcing the atomised working fluid from the
8	first transport fluid passage into a second
9	transport fluid passage via one or more second
10	communicating bores extending radially outwardly
11	from the first transport fluid passage;
12	supplying a second transport fluid through the
13	second transport fluid passage;
14	accelerating the second transport fluid
15	upstream of the second communicating bores so as to
16	provide a second high velocity transport fluid flow;
17	and
18	applying the second high velocity transport
19	fluid flow to the atomised working fluid exiting the
20	second communicating bores, thereby imparting a
21	second shear force on the atomised working fluid and
22	further atomising the working fluid;
23	wherein the second high velocity transport
24	fluid flow is applied substantially perpendicular to
25	the atomised working fluid flow exiting the second
26	bores.
27	
28	Preferred embodiments of the present invention will
29	be described, by way of example only, with reference
30	to the accompanying drawings, in which:
31	

1	Figures 1(a)-1(e) show detail section views
2	through a first embodiment of a mist generating
3	apparatus;
4	Figure 2 shows a detail section view through a
. 5	second embodiment of a mist generating apparatus;
6	Figure 3 shows a section view through a third
7	embodiment of a mist generating apparatus;
8	Figures 4(a)-4(c) show detail section views
9	through a fourth embodiment of a mist generating
10	apparatus;
11	Figure 5 shows a detail section view through a
12	fifth embodiment of a mist generating apparatus;
13	Figure 6 shows a detail section view through a
14	sixth embodiment of a mist generating apparatus; and
15	Figure 7 shows a detail section view through a
16	seventh embodiment of a mist generating apparatus.
17	
18	Figure 1(a) shows a first embodiment of mist
19	generating apparatus according to the present
20	invention. The apparatus, generally designated 10,
21	comprises a generally cylindrical body 12 and an
22	elongate member 14 projecting co-axially within the
23	body 12. The member 14 and body 12 are so arranged
24	that a first transport fluid passage 16 and a nozzle
25	32 are defined between the two. The body 12 has an
26	internal wall 18 which includes a convergent portion
27	20 upstream of a divergent portion 22. The elongate
28	member 14 has an external wall 24 which is
29	substantially straight and parallel to the
30	longitudinal axis L shared by the body and elongate
31	member. As Figure 1(a) is only a detail view, it
32	will be appreciated that the entire apparatus is not

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illustrated in this figure. As the body 12 is 1 2 generally cylindrical, a further portion of the body 12, mirrored about the longitudinal axis L, is 3 present below the elongate member 14, but is not 4 shown in Figure 1(a) for reasons of clarity. · 5 passage 16 is an annular passage surrounding the 6 elongate member 14. The elongate member 14 ends in 7 a cone-shaped projection 15. R 9 The elongate member 14 includes a passage 26 for the 10 The passage will introduction of a working fluid. 11 therefore be referred to as the working fluid 12 passage 26. The passage 26 extends along the length 13 of the elongate member 14 and is also co-axial with 14 the body 12 and elongate member 14. The passage 26 15 is blind, in that it ends in a cavity 28 located in 16 the outer cone portion 15 of the elongate member 14. 17 Extending radially outwardly from the passage 26 in 18 a direction substantially perpendicular to the 19 transport fluid passage 16 are one or more 20 communicating bores 30. These bores 30 allow fluid 21 22 communication between the working fluid passage 26 and the transport fluid passage 16. The outer cone 23 portion 15 of the elongate member 14 and the 24 divergent portion 22 of the internal wall 18 define 25 a mixing chamber 19 which opens out into a nozzle 32 26 through which fluid is sprayed. 27 28 29 The operation of the first embodiment will now be described. A working fluid, such as water for 30 example, is introduced from a working fluid inlet 31

(not shown) into the working fluid passage 26.

_	working fluid flows along the passage 26 until
2	reaching the cavity 28. Upon reaching the cavity
3	28, the working fluid is forced through the bores 30
4	into the transport fluid passage 16. A transport
5	fluid, such as steam for example, is introduced from
б	a transport fluid inlet (not shown) into the
7	transport fluid passage 16. Due to the convergent-
8	divergent section of the passage 16 formed by the
9	convergent and divergent portions 20,22 of the body
10	18, the passage acts as a venturi section,
11	accelerating the transport fluid as it passes
12	through the convergent-divergent section into the
13	mixing chamber 19. This acceleration of the
14	transport fluid ensures that the transport fluid
15	flows past the ends of the bores 30 at very high,
16	possibly even supersonic, velocity.
17	
18	With the transport fluid flowing at such high
19	velocity and the working fluid exiting the bores 30
20	into the passage 16 in a direction substantially
21	perpendicular to the transport fluid flow, the
22	working fluid is subjected to very high shear forces
23	by the transport fluid. Droplets are sheared from
24	the working fluid flow as it exits the bores 30
25	producing a dispersed droplet flow regime. The
26	atomised flow is then carried out through the mixing
27	chamber 19 to the nozzle 32. In such a manner, the
28	apparatus 10 creates a flow of substantially uniform
29	sized droplets from the working fluid.
30	
31	Figures 1(b)-1(e) show potential modifications to
32	the nozzle 32 adjacent the outlet of the bores 30.

Figures 1(b)-1(d) show nozzles where the outlet of 1 2 the bore 30 has a greater cross-sectional area than the inlet 29 communicating with the working fluid 3 4 passage 26. In Figure 1(b) the bore 30 has a curved 5 outward taper at the outlet 31b which provides the outlet 31b with a bowl-shaped profile when viewed in 6 In Figure 1(c), a similar arrangement is 7 shown, but here the expanded diameter of the outlet 8 9 31c is achieved by providing a stepped portion rather than a gradual outward taper. With the 10 nozzle of Figure 1(d), the bore 30 gradually tapers 11 12 outwards along the length thereof from inlet 29 to 13 outlet 31d. 14 15 By providing bores 30 whose outlets 31b,31c,31d are 16 of greater diameter than their respective inlets 29, 17 an area of lower pressure is provided in the working 18 fluid as it leaves the outlets 31b,31c,31d. 19 has the effect of presenting a greater surface area 20 of working fluid to the transport fluid in the 21 mixing chamber 19, thereby further increasing the shear effect of the transport fluid on the working 22 23 fluid. Additionally, the expansion of the bores 30, particularly in the cases of the Figure 1(b) and 24 25 1(c) nozzles, will increase the turbulence of the 26 working fluid flow as it exits the bores 30, 27. limiting the potential for any of the working fluid 28 flow to become trapped along the walls of the bores 29 30. 30 31 As explained above, one undesirable phenomenon in mist generating apparatus is that some of the 32

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1 working fluid is not instantly atomised upon exit 2 from the bores 30. In such instances, the nonatomised fluid can flow along the wall of the outer 3 4 cone portion 15 of the nozzle 32 and then disrupt 5 the size of the working fluid droplets which have 6 already been atomised. This phenomenon can be 7 avoided in the nozzle shown in Figure 1(e). With this nozzle, the wall of the outer cone portion 15 8 9 is provided with a ramped portion 34 which extends 10 upwardly from the outer cone wall to a peak, also known as a surface separation point. Any non-11 12 atomised fluid flow along the outer cone 15 will 13 flow up the ramped portion 34. Once the fluid flow 14 arrives at the peak, it will be subjected to the 15 shear forces of the transport fluid, will atomise, and then join the remainder of the droplets as they 16 17 exit the nozzle 32. 18 19 Figure 2 shows a second embodiment of the apparatus, 20 which also solves the same problem as the modified 21 nozzle of Figure 1(e). In this instance, the 22 elongate member 14 includes a working fluid passage 23 26 as before. However, instead of passing through 24 the central axis of the elongate member 14 as in the 25 previously described embodiments, in this embodiment the working fluid passage 26 is arranged so as to 26 27 circumscribe a second transport fluid passage 40 located along the longitudinal axis of the elongate 28 29 member 14. The purpose of the second transport 30 fluid passage 40 is to ensure any non-atomised fluid which flows down the surface of the outer cone 15 is 31

atomised when it reaches the outlet 42 of the

1 passage 40, which is adjacent the end of the outer 2 cone 15. Thus, transport fluid flows through both the first transport fluid passage 16 and the second 3 transport fluid passage 40. The second transport fluid passage 40 can include an expansion chamber 44 5 6 if desired, and is preferably substantially parallel 7 to the first transport fluid passage 16. 8 A third embodiment of the apparatus is shown in 9 This embodiment shares a number of 10 Figure 3. 11 features with the first embodiment described above. As a result, these features will not be described 12 again in detail here, but have been assigned the 13 14 same reference numbers, where appropriate. first difference between the first and third 15 16 embodiments is that the external wall 24' of the 17 elongate member 14 is of the same convergent-18 divergent geometry as the internal wall 18 of the 19 body 12. Hence, the convergent and divergent 20 portions 20,22 of the internal wall 18 are mirrored 21 by identical portions of the external wall 24' of 22 the elongate member 14. As a result, both walls 23 18,24' define a throat section 50 in the first 24 transport fluid passage 16. 25 26 The second key difference between the third 27 embodiment of the apparatus and the preceding 28 embodiments is that as well as having a first 29 working fluid passage 26 along the centre of the 30 elongate member 14, a second working fluid passage 52 is also provided in the body 12, the second 31 . 32 working fluid passage 52 circumscribing both the

•	Tirst working ridid passage 20 and the transport
2	fluid passage 16. This means that working fluid is
3	supplied into the mixing chamber 19 from both first
4	and second bores 30,54 which extend radially
5	outwardly from their respective passages 26,52 and
6	connect the first and second working fluid passages
7	26,52 with the transport fluid passage 16. As with
8	the first working fluid passage 26, the second
9	working fluid passage 52 is also blind, with a
10	cavity 56 located at the end of the passage 52
11	remote from the working fluid inlet (not shown).
12	The first and second bores 30,54 are preferably co-
13	axial, as seen in section in Figure 3. This ensures
14	that the working fluid enters the transport fluid
15	passage 16 at the same point from both the first and
16	second working fluid passages 26,52. The first and
17	second bores 30,54 are substantially perpendicular
18	to the transport fluid passage 16.
19	
20	The third embodiment will operate in substantially
21	the same manner as that described in respect of the
22	first embodiment. Working fluid exiting the first
23	and second bores 30,54 will be sheared by the
24	transport fluid flowing through the transport fluid
25	passage 16, thereby creating a mist of uniform sized
26	droplets.
27	
28	A fourth embodiment of the invention is illustrated
29	in Figure 4(a). Again, the basic layout of the
30	apparatus is the same as with the first embodiment,
31	so like features have been again assigned the same
32	reference numbers. The elongate member 14 has a

1 central working fluid passage 26 which ends in a 2 cavity 28 remote from a working fluid inlet (not shown). A first transport fluid passage 16 is 3 defined by an external wall 24 of the elongate 4 5 member 14 and convergent and divergent portions 20,22 of the internal wall 18 of the body 12. 6 Again, it will be appreciated that Figure 4(a) only 7 8 illustrates half of the apparatus, with the half not 9 illustrated being a mirror image about the 10 longitudinal axis L of the illustrated portion. 11 The elongate member 14 of this fourth embodiment is 12 13 adapted to include a second transport fluid passage 14 60 circumscribing the central working fluid passage The transport and working fluid passages 60,26 15 are co-axial about the longitudinal axis L. 16 the second transport fluid passage 60 circumscribing 17 18 the working fluid passage 26, the second transport 19 fluid passage lies between the working fluid passage 20 26 and the first transport fluid passage 16. number of first bores 62 allow fluid communication 21 between the working fluid passage 26 and the second 22 23 transport fluid passage 60. A number of second bores 64 allow fluid communication between the 24 second transport fluid passage 60 and the first 25 26 transport fluid passage 16. 27 In operation, working fluid is forced through the 28 first bores 62 into the second transport fluid 29 passage 60, where transport fluid shears the working 30 31 fluid entering the passage perpendicular to the

transport fluid flow. The resultant atomised fluid

1	then flows through the second bores 64 into the
2	first transport fluid passage 16, whereupon it is
3	sheared for a second time by a second flow of
4	transport fluid. Providing two locations at which
5	the working fluid is subjected to the shear forces
6	of the transport fluid allows the apparatus to
7	generate still smaller droplet sizes.
8	
9	Figures 4(b) and 4(c) illustrate examples of
10	communicating bores 70,72 which are not
11	perpendicular to the flow of transport fluid through
12	the transport fluid passage 16. The bore 70 of
13	Figure 4(b) presents fluid into the transport fluid
14	flow at an angle of less than 90 degrees such that
15	the fluid flows against the flow of transport fluid
16	Such an arrangement increases the shear forces on
17	the working fluid from the transport fluid. In
18	Figure 4(c) the bore 72 is at an angle of over 90
19	degrees, so that the fluid flow is at an angle to
20	the transport fluid flow, but is not perpendicular
21	thereto. This arrangement reduces the amount of
22	shear imparted on the working fluid by the transport
23	fluid.
24	
25	A fifth embodiment of the invention is illustrated
26	in Figure 5. The elongate member 14 has a central
2 <b>7</b>	working fluid passage 26 which ends in a cavity 28
28	remote from a working fluid inlet (not shown). A
29	first transport fluid passage 16 is defined by an
30	external wall 24 of the elongate member 14 and
31	convergent and divergent portions 20,22 of the
12	internal wall 18 of the body 12. In this

17

1 embodiment, the external wall 24 of the elongate 2 member 14 tapers outwardly in the direction of the 3 mixing chamber 19 and nozzle 32 until it reaches one or more second bores 64. Again, it will be 4 5 appreciated that Figure 5 only illustrates half of 6 the apparatus, with the half not illustrated being a 7 mirror image about the longitudinal axis L of the illustrated portion. 8 9 The elongate member 14 of this fourth embodiment is 10 adapted to include a second transport fluid passage 11 12 60 circumscribing the central working fluid passage 13 The transport and working fluid passages 60,26 are co-axial about the longitudinal axis L. With 14 the second transport fluid passage 60 circumscribing 15 16 the working fluid passage 26, the second transport fluid passage lies between the working fluid passage 17 18 26 and the first transport fluid passage 16. One or more first bores 62 allow fluid communication 19 between the working fluid passage 26 and the second 20 21 transport fluid passage 60. One or more of the 22 second bores 64 allow fluid communication between 23 the second transport fluid passage 60 and the first 24 transport fluid passage 16. 25 A further difference between the fifth embodiment 26 27 and the preceding fourth embodiment in particular is 28 that a third transport fluid passage 80 is provided 29 in the elongate member 14. The third transport 30 fluid passage 80 may receive transport fluid from the same source as the first and second transport 31

fluid passages 16,60, or else it may have its own

1 dedicated transport fluid source (not shown). 2 third transport fluid passage 80 has an outlet 82 which is on the downstream side of the first bore(s) 3 62. As a result, the outlets of the second and 4 third transport fluid passages 60,80 are positioned 5 6 either side of the first bores 62 and open into the 7 second bores 64. 8 9 In operation, working fluid is forced through the 10 first bores 62 from the working fluid passage 26, where transport fluid from the second and third 11 12 transport fluid passages 60,80 shears the working 13 The resultant atomised fluid then flows 14 through the second bores 64 into the first transport fluid passage 16, whereupon it is sheared for a 15 16 second time by a second flow of transport fluid. 17 Providing two locations at which the working fluid 18 is subjected to the shear forces of the transport 19 fluid allows the apparatus to generate still smaller 20 droplet sizes. By providing two sources of 21 transport fluid from the second and third transport 22 fluid passages 60,80 adjacent the first bore(s) 62, 23 even smaller droplets of the working fluid can be 24 obtained due to the effective twin shear action of 25 the transport fluid on the working fluid prior to the atomised fluid entering the second bore(s) 64 26 and being further atomised. **27** ' 28 29 Figures 6 and 7 show sixth and seventh embodiments 30 of the apparatus, respectively, in which secondary 31 shear actions take place in the manner of the fourth and fifth embodiments described above. 32

1 embodiment shown in Figure 6, the elongate member 14 2 has a central working fluid passage 26 which ends in a cavity 28 remote from a working fluid inlet (not 3 shown). A first transport fluid passage 16 is 4 5 defined by an external wall 24 of the elongate member 14 and convergent and divergent portions 6 20,22 of the internal wall 18 of the body 12. The external wall 24 of the elongate member 14 runs 8 9 substantially parallel to the transport fluid passage 26. One or more first bores 62 allow fluid 10 11 communication between the working fluid passage 26 and the first transport fluid passage 16. 12 13 The key difference between the sixth embodiment and 14 the fifth embodiment in particular is that a second 15 transport fluid passage 90 is provided, but in this 16 17 case the second transport fluid passage 90 is substantially perpendicular to the first transport 18 fluid passage 16. The second transport fluid 19 20 passage 90 may receive transport fluid from the same 21 source as the first transport fluid passage 16, or 22 else it may have its own dedicated transport fluid source (not shown). In this embodiment, the first 23 24 transport fluid passage 16 has an outlet 17 in 25 communication with the second transport fluid 26 passage 90. A mixing chamber 19 is defined where the first and second transport fluid passages 16,90 27 meet one another. The second transport fluid 28 passage 90 has a convergent-divergent internal 29 30 geometry upstream of the first transport fluid passage outlet 17, thereby ensuring that the 31 transport fluid passing through the passage 90 is 32

accelerated prior to meeting the atomised fluid
exiting the first transport fluid passage 16.

3

In operation, working fluid is forced through the

5 first bores 62 from the working fluid passage 26,

6 where transport fluid from the first transport fluid

7 passage 16 shears the working fluid. The resultant

3 atomised fluid then flows through the outlet 17 into

9 the second transport fluid passage 90, whereupon it

10 is sheared for a second time by the second flow of

11 transport fluid.

12

13 The seventh embodiment of the invention differs from

14 the sixth embodiment in that the second transport

15 fluid passage 100 is arranged such that the

16 direction of the second transport fluid flow is

17 generally opposite to the flow of transport fluid

18 through the first transport fluid passage 16. As

19 before, both the first and second transport fluid

20 passages 16,100 have convergent-divergent internal

21 geometry.

22

23 Working fluid exits the working fluid passage 26 via

24 first bore(s) 62 in a flow direction perpendicular

25 to the first transport fluid passage 16. Transport

26 fluid accelerated through the passage 16 shears the

27 working fluid exiting the bore(s) 62, creating an

28 atomised fluid flow. The atomised fluid flow,

29 flowing in the direction indicated by arrow D1, then

30 meets the accelerated secondary transport fluid

31 flow, illustrated by arrow D2, at a mixing chamber

32 19. The two fluid flows D1, D2 combine in the mixing

1 chamber 19 to further atomise the working fluid prior to the atomised working fluid exiting via 2 outlet 104. 3 5 The purpose of the sixth and seventh embodiments is to shear the working fluid once and then carry the droplets into a further stream of transport fluid 7 where the velocity of the droplets is reduced. 8 9 allows the production of uniform droplets by shearing with a first, preferably supersonic, stream 10 of transport fluid and then reducing the velocity of 11 the stream with the second transport fluid flow. 12 13 These embodiments are for use in applications which require small droplet size but low projection 14 15 velocities. 16 17 Each of the embodiments described here uses the generally perpendicular arrangement of the working 18 19 fluid bores and transport fluid passages to obtain a 20 crossflow of the transport and working fluids. 21 crossflow (where the two fluid flows meet at 22 approximately 90 degrees to one another) ensures the penetrative atomisation of the working fluid as the 23 24 transport fluid breaks up the working fluid. 25 natural Kelvin-Helmholtz/Rayleigh Taylor instabilites in the working fluid as it is forced 26 into an ambient pressure environment also assist the 27 atomisation of the working fluid. 28 29 30 Furthermore, by locating the elongate member 14 along the centre of the apparatus, the atomised 31 working fluid exits the apparatus via an annular 32

nozzle which circumscribes the elongate member. 1 2 elongate member effectively blocks the centre of the nozzle, which provides a further geometric mechanism 3 4 to assist the atomisation of the working fluid. 5 blocking of the centre of the nozzle creates a low 6 pressure recirculation zone adjacent the nozzle cone 7 As the high-speed atomised working fluid exits the annular nozzle it imparts further shear forces 8 9 on the droplets in the recirculation zone, leading 10 to a further atomisation of the working fluid. 11 In the fifth embodiment shown in Figure 5, the 12 13 method of operation may be adapted by swapping the 14 functions of the fluid passages 26,60,80. 15 words, the passage 26 could supply the transport 16 fluid, whilst the passages 60,80 supply the working 17 fluid. In an alternative adaptation of the 18 apparatus of the fifth embodiment, the apparatus 19 could be adapted to feed gas bubbles through the 20 first bores 62 as the working fluid passes through. 21 This has the effect of breaking up the working fluid 22 stream prior to atomisation and also increasing 23 turbulence in the working fluid, both of which help 24 improve the atomisation of the working fluid in the 25 apparatus. 26 27 Further modifications and improvements may be 28 incorporated without departing from the scope of the 29 invention.

